This listing of claims will replace all prior versions, and listings, of claims in the application.

- 1. (Currently Amended) Apparatus for the production of cement clinker with

  [[a.]] a heat exchanger (I) for the for the preheating of raw meal (2) raw meal,

  [[b.]] a kiln (3) a kiln for the final burning of the cement clinker, wherein the exhaust
- exhaust gases from the kiln flow through the heat exchanger,
- [[c.]] a catalytic converter (5) which is converter, disposed in the direction of flow of the exhaust gases after the heat exchanger and exchanger, for reaction of NO with CO, and [[d.]] means (6, 7) means for the analysis of the exhaust gases before and/or after the catalytic converter,

characterised in that a calciner (4) is further provided for the the apparatus further comprising a calciner for precalcination of the preheated raw meal.

- 2. (Currently Amended) Apparatus as claimed in Claim 1, characterised characterized in that the calciner (4) has means (41,42, 43) has means for the staged delivery of fuel and/or means (44, 45) for the staged delivery of air for combustion.
- 3. (Currently Amended) Apparatus as claimed in Claim 1, characterised characterized in that the calciner (4) calciner has an additional combustion chamber (47) chamber through which the exhaust gases from the kiln do not flow.

- 4. (Currently Amended) Apparatus as claimed in one or more of Claims 1, characterized in that the calciner (4) calciner has means (46) means for the staged delivery of preheated raw meal.
- 5. (Currently Amended) Apparatus as claimed in Claim 1, characterised characterized in that a flow rectifier (10) rectifier is disposed upstream of the catalytic converter in the direction of flow of the exhaust gases.
- 6. (Currently Amended) Apparatus as claimed in Claim 1, characterised characterized in that a separating stage (15) stage for heavy metals is disposed between the heat exchanger (1) exchanger and the catalytic converter (5) converter.
- 7. (Currently Amended) Apparatus as claimed in Claim 1, characterised characterized in that the heat exchanger comprises a plurality of cyclone stages which are disposed one above the other, wherein the raw meal flows through the individual cyclone stages from top to bottom whilst the exhaust gases (8) gases pass through the cyclone stages from bottom to top, and wherein furthermore a material deflector (9) deflector is provided in order to deliver a proportion of the raw meal in the region of the uppermost cyclone stage (1a) and a proportion in the region of the cyclone stage (1b) stage which lies below it.
- 8. (Currently Amended) Apparatus as claimed in Claim 1, characterised characterized in that means are provided in order to introduce exhaust air (13) exhaust air from a clinker

exchanger and the catalytic-converter (5) converter.

- 9. (Currently Amended) Apparatus as claimed in Claim 1, characterised characterized in that means (50) means are provided in order to introduced a reducing agent, in particular an ammonium carrier and/or hydrocarbon, in the region of the calciner and/or the heat exchanger.
- 10. (Cancelled)
- 11. (Currently Amended) Apparatus as claimed in Claim 1, <del>characterised in that a fan (16) characterized in that a fan is disposed between the heat exchanger (I) exchanger and the catalytic converter (5) converter.</del>
- 12. (Currently Amended) Method of producing cement clinker, wherein raw meal (2) meal is preheated in a heat exchanger (I) exchanger and is burnt in a kiln (3) kiln to form cement clinker and the and exhaust gases (8) gases from the kiln flow in succession through the heat exchanger and a catalytic converter (5), converter, and the exhaust gases being analysed are analyzed before and/or after the catalytic converter, characterised in that and wherein a catalytic converter reaction of NO with CO is used, and the CO content is tailored specifically to the catalytic converter by the combustion conditions in the calciner and/or by the addition of further fuel wherein the preheated raw meal is precalcined in a calciner (4) calciner.

- 13. (Currently Amended) Method as claimed in Claim 12, characterised characterized in that the heat exchanger (I) exchanger comprises a plurality of cyclone stages (1a, 1b, 1c) which are disposed one above the other, wherein the raw meal (2) meal passes through the individual cyclone stages from top to bottom whilst the exhaust gases (8) gases flow through the cyclone stages from bottom to top, wherein the raw meal is divided up as a function of the temperature of the exhaust gases flowing through the catalytic converter (5) converter and is supplied in the region of two different cyclone stages.
- 14. (Currently Amended) Method as claimed in Claim 12, characterised in that the calciner (4) calciner is operated with a staged combustion and/or a staged delivery of air and/or a staged supply of raw meal.
- 15. (Currently Amended) Method as claimed in Claim 12, characterised in that a reducing agent, in particular an ammonium carrier and/or a hydrocarbon, is introduced in the region of the calciner (4) calciner and/or the heat-exchanger (I) exchanger.
- 16. (Currently Amended) Method as claimed in Claim 15, characterised characterized in that the quantity of reducing agent to be introduced is adjusted according to the analysis of the exhaust gases measured before and/or after the catalytic-converter (5) converter.

- 17. (Cancelled)
- 18. (Currently Amended) Method as claimed in Claim 12, characterised characterized in that a proportion of the exhaust gases from the kiln is discharged before the calciner (4) calciner, cooled and freed of dust and then is fed back to the exhaust gases before the catalytic-converter (5) converter.
- 19. (Currently Amended) Method as claimed in Claim 12, characterised characterized in that a proportion of the exhaust gases is discharged in the direction of flow after the heat-exchanger (1), exchanger is delivered to a coal mill (19) coal mill and a dust removal means (20) means and then is fed back to the exhaust gases before the catalytic converter (5) converter.